

Please amend the specification as follows:

Page 2, line 19,

-- The applicant has developed a process to obtain polyglycolyl urea hydantoin from aromatic diglycinates, the main characteristic of which is that it does not form high risk polluting residual by-products such as HCN emission, obtaining a product that meets the main properties of such commercially available resins such as thermal, mechanical, and chemical properties and even improving certain characteristics such as freon resistance of polyesterimide-type enameled products.-

Page 3, lines 4 and 6:

Hereinafter the invention will be described according to the process stages to obtain the polyglycolyl urea hydantoin as well as its use, main object of the application, in the manufacturing of H-class magnet-wire with improved properties.

The process to obtain polyglycolyl urea hydantoin PGU is divided in two main stages A and B.--

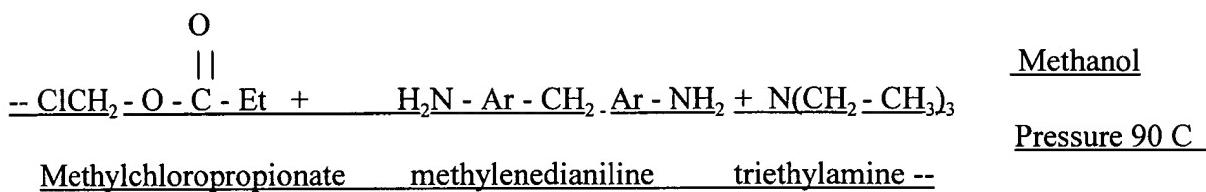
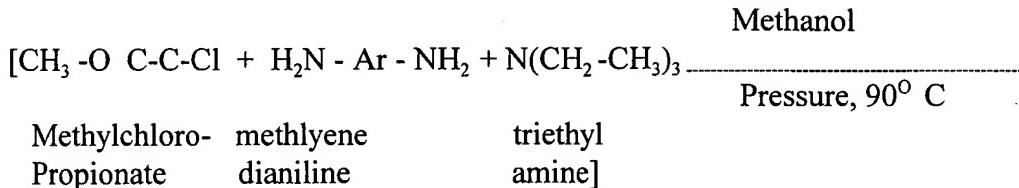
Page 3, lines 14 and 16:

--Stage B includes the following steps:

- 4) loading [aromatic] methyl isocyanate, diglycinate, solvents and catalyst in the polymerization reactor;
- 5) obtaining polyglycolyl urea hydantoin resin;
- 6) adding polyester-type electro-insulating varnishes;
- 7) manufacturing H-class magnet-wire with improved properties. --

Page 4, lines 19 - 22 (end of the page), please delete the lines and replace with the following:

-- Path 2: nucleophilic shift



Page 5, line 12, please add the following:

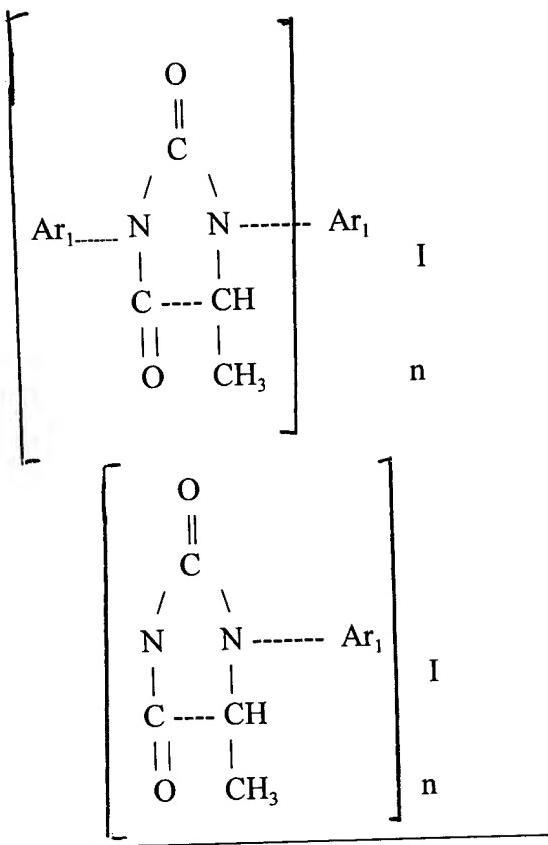
Obtainment of methyl diglycinate from methylenedianiline

a) [in] In a glass or stainless steel matrass, provided with stirring means, reflux column, heating and cooling systems, the following materials are added: methylenedianiline, methanol, and methyl bromopropionate. A C₁-C₄ aliphatic solvent may be used.

Page 7, beginning at line 4, please make the following amendment:

Once the theoretical distillate is recovered, heating is stopped, and the resin is cooled at 70° C to unload the corresponding containers, and a polyglycolyl urea hydantoin resin of the following

formula is obtained:



where Ar₁ is a substituted aromatic compound or a substituted diphenylalkyl, and 2< n <500,

% solids = 28.97

IN THE CLAIMS

Claims 1-5 (previously canceled).

Claims 6-11 (canceled).

Claim 12 (previously canceled)

Claims 13-23 (canceled)

Claim 24 (previously canceled)

Claim 25 (previously canceled)

Claim 26 (canceled)

Add the following claims:

-27 (new). A process for obtaining polyglycolyl urea resin from aromatic diglycinates for insulating electric conductor, in the absence of HCN polluting residues, comprising the following steps:

A) preparing a methyl diglycinate:

a) reacting a mixture of methylhaloester and methylenedianiline in the presence of C₁—C₄ aliphatic solvent under reflux conditions at atmospheric pressure and up to solvent reflux temperature of 58 – 63°C;

b) adding triethylamine, as catalyst at a rate of 0.178 l/hr. per Kg of reactants;

c) separating the solvent through atmospheric distillation till 40% of its initial volume is recovered;

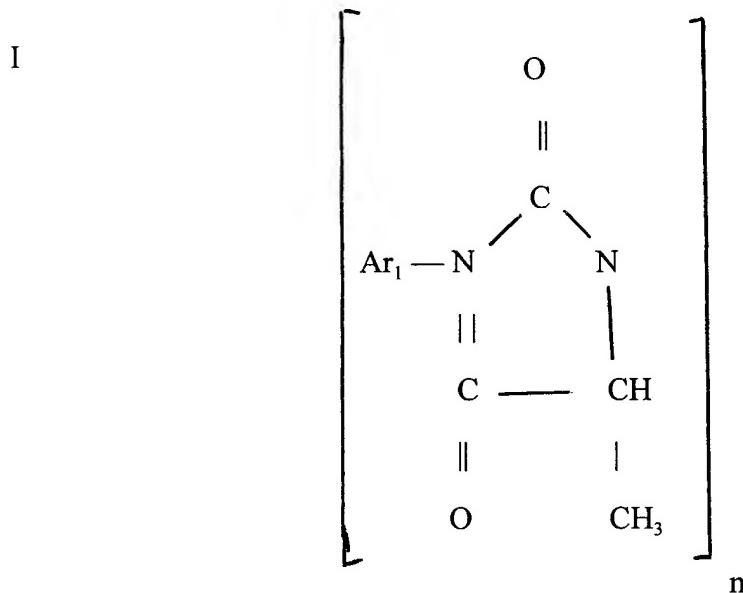
d) cooling at 20 °C under stirring and beginning at 50°C

e) filtering and purifying the diglycinate by washing with water;

f) drying the methyl diglycinate obtained;

B) preparing polyglycolyl urea resin:

- a) reacting the obtained diglycinate with aromatic isocyanate in the presence of a solvent as cresylic acid in a reactor until solution is complete at 60 °C;
- b) reacting the diglycinate preferable with metilen diisocyanate solvent and catalyst at a temperature of 200°C;
- c) distilling and then cooling the reaction product; and
- d) recovering the polyglycolyl urea resin having the formula I:



where Ar_1 is a substitute aromatic compound such as a substitute diphenylalkyl, and $2 < n \leq 500$.

28. (new) The process according to claim 27 wherein the methylhaloester is selected from the group consisting of methylbromopropionate and methylchloropropionate.

29. (new) The process according to claim 27 wherein the mixture reflux is conducted for at least 16 hours

30.(new) The process according to claim 27 wherein the triethylamine is added at a rate of 0.178 l/hr per Kg of product during a 3-5 hour period

31. (new) The process according to claim 27 A(h) wherein the reaction is increased up to temperature of 200°C

32. (new) The process according to claim 27 wherein the resin obtained is cooled at 70°C

33. (new) The process according to claim 27 wherein the catalyst in step (h) is selected from the group consisting of tretylenediamino and 1,4 diazobicyclo (2,2,2) octane and is added at temperatures up to 180 °C

34.(new) The process according to claim 27 wherein the polyglycolyl urea resin obtained has viscosity (Cp) of 4,800 at 15% solids.

35. (new) The process according to claim 27, wherein the C₁—C₄ aliphatic is methanol.

36. (new) The process according to claim 27, wherein the aromatic diglycinate is preferable a methyl diglycinate obtained and is dried with hot air at 40°C and corresponds to a stereoisomer mixture with a melting point of 95 – 116°C of the following formula II:

